

Biodiesel Production Technologies

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Biofuels Activities of IFC, Uni Graz Department of Renewable Resources

- Development of biodiesel process technologies
- Alternative feedstocks for biodiesel production
- Alternative uses for biodiesel and side products
- Research on analysis and characterization of fats and oil derivatives
- Development of specifications
- Training and seminars on biodiesel analysis and quality management
- Research on second generation biofuels: BTL, biomethanol, ...



First Laboratory Experiments 1981



1986: Mittelbach, Junek, Andreae: AT 386.222

IFC: Over 25 Years Experience in Biodiesel



1987: 1st pilot plant worldwide for Biodiesel: Silberberg, Styria, Austria

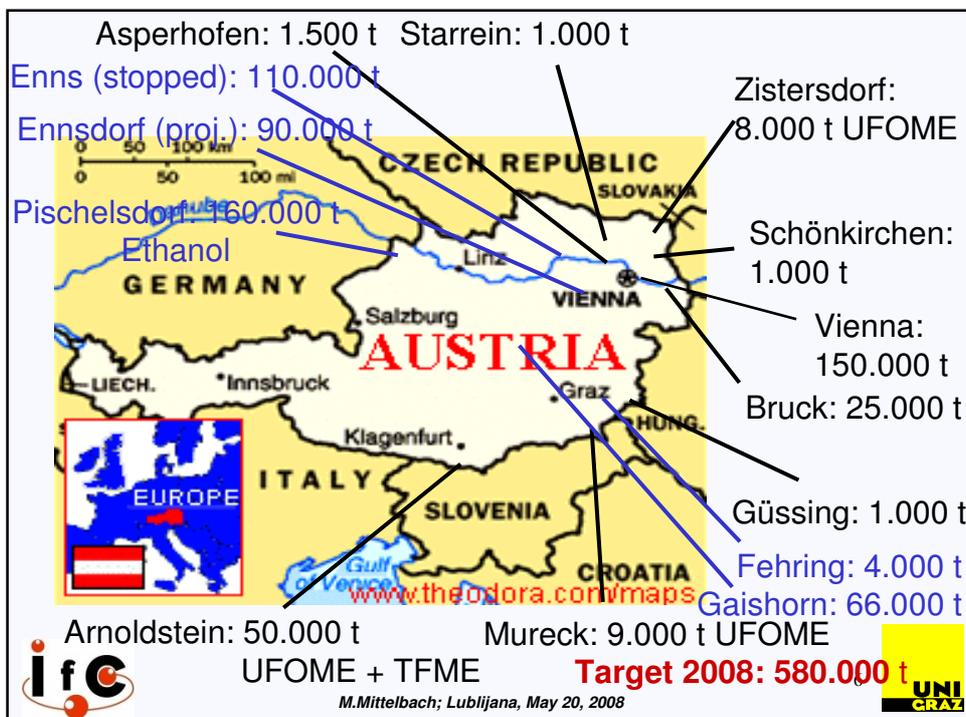


1st Biodiesel Plant in a European Capital, BDV Vienna, 2006



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Feedstocks for Biodiesel Production

First Generation:

Vegetable food oils: rape seed, palm, soybean, sunflower

Second Generation:

„New“ seed oils

Cuphea, camelina, crambe, cotton seed, GMO

Non-edible seed oils

Jatropha curcas, castor oil, karanja....

Waste oils and fats

Used frying oil, tallow, soap stock, trap grease

Third Generation:

Single cell oils: algae



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1983:

First Experiments
With Used Frying Oil

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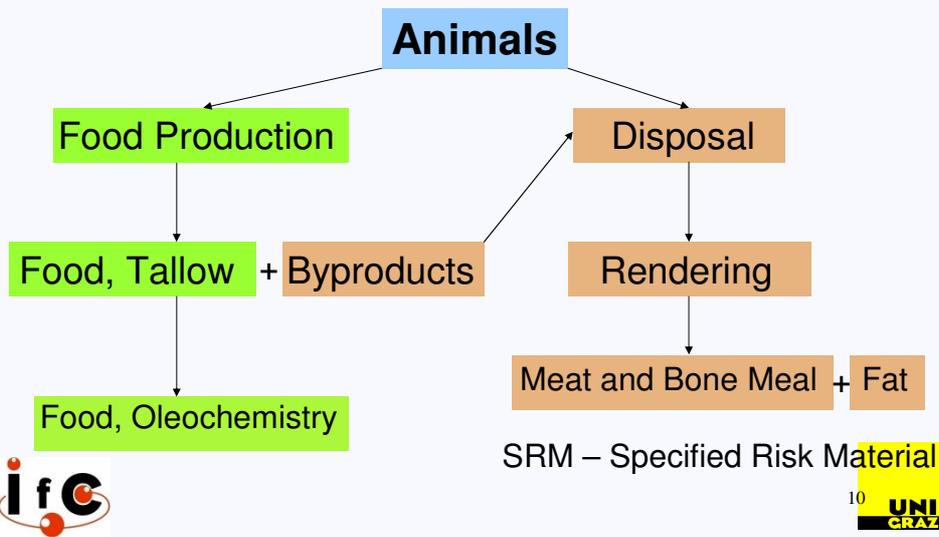


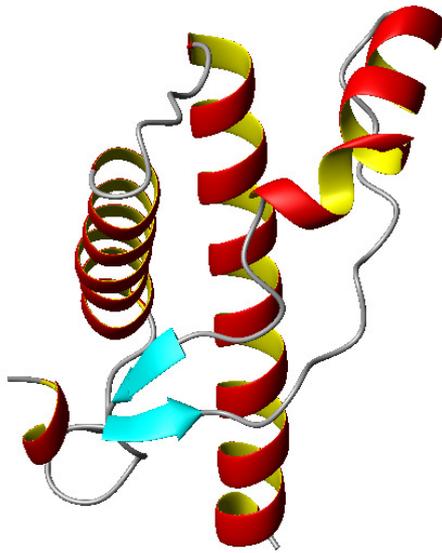
All 150 City Buses in Graz are running with **ÖKODRIVE**[®]
 100 % Biodiesel from Used Frying Oil



World Climate Star 2002
 Osmose Award 2006

Animal Byproducts as Feedstock





Prion protein
responsible for
BSE disease:

Destruction during
Biodiesel process?



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European Food Safety Authority (EFSA)

The Scientific Panel on Biological Hazards concludes
that the Biodiesel process as described (BDI)
is considered as safe for treatment
and use of ABP of category 1



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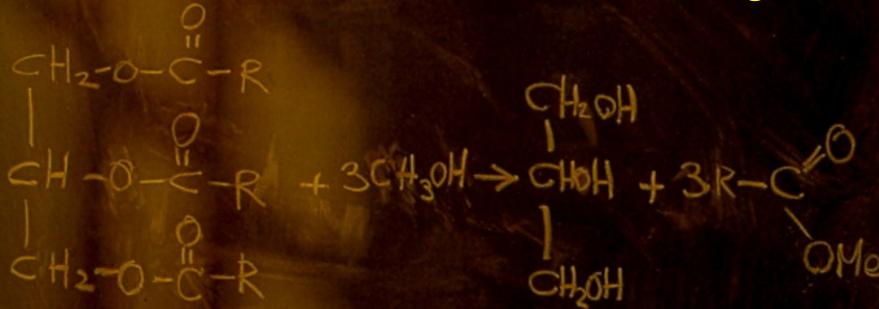




Algae for Biodiesel Production



Kronenzeitung, 1991



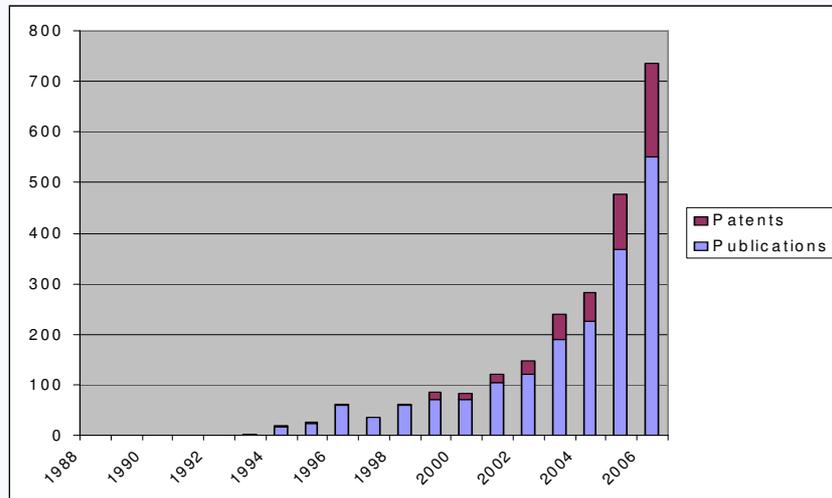
Die Formel für nachwachsenden Diesel

History of Alcoholysis of Triacylglycerols

- 1852 *P.Duffy: Alcoholysis of fats: J.Chem.Soc.*
- 1944 *G.B.Bradshaw: US 2,360,844*
preparation of pure glycerol: 2-step reaction
- 1950 ff Fatty alcohol production for nonionic detergents
high temperature and pressure process
240 °C; 100 bar; NaOCH₃; distillation
- 1986 *Mittelbach et al. AT 386.222*
low temperature and pressure process for
biodiesel production: KOH; purification with IER
- 1990 ff over 200 patents on biodiesel production



Citations in Chemical Abstracts „Biodiesel“



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Biodiesel Production Technologies

1) Single Feedstock Technologies

Feedstock	→	Fully refined vegetable oils, FFA < 1 %
Catalyst	→	NaOCH ₃ , NaOH, KOH
Reaction conditions	→	40-100 °C, batch or continuous
Purification ME-Ester	→	water washing, drying, no distillation
Glycerol treatment	→	removal H ₂ O+MeOH, opt.: distillation
Capacity	→	500 t – 250.000 t/a



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Biodiesel Production Technologies

2) Multi Feedstock Technologies

FFA: up to 100 %

Feedstock → Crude vegetable oils, animal fat, waste oils

Catalyst → Preesterif.: H⁺; Transesterif.: KOH

Reaction conditions → 40-60 °C, batch or continuous

Purification ME-Ester → water washing, drying, distillation

Glycerol treatment → acidification, salt separation: crude glycerol

Capacity → 5.000 t – 50.000 t/a



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Homogenous Catalysts for Transesterification

Type of Catalyst	Comments
Sodium hydroxide	Cheap, disposal of residual salts necessary
Potassium hydroxide	Reuse as fertilizer possible, fast reaction rate, better separation of glycerol
Sodium methoxide	No dissolution of catalyst necessary, disposal of salts necessary disposal
Potassium methoxide	No dissolution of catalyst necessary, fertilizer, better separation of glycerol, high price



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Acidic Catalysts for Esterification

Type of Catalyst	Comments
Conc. sulphuric acid	Cheap, decomposition products, corrosion
p-Toluene-sulphonic acid	High price, recycling necessary
Acidic ion exchange resins	High price, continuous reaction possible, low stability



New Trends: Heterogenous Catalysts

Metal oxides (Mg, Ca, Al, Fe)
Carbonates: CaCO_3
Ion exchange resins (acidic, alkaline)
Enzymes
Silicates

- + easy separation, reusable
pure glycerol, no side products (salts)
first industrial application 2006
- high temperature and pressure, high investment costs



New Trends: Enzymes as Catalysts

Lipases (Triacylglycerolhydrolases)

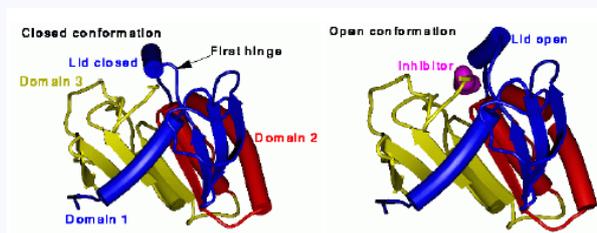
main task: lipid hydrolysis

in organic solvents:

esterification, transesterification

Alcoholysis of sunflower oil with MeOH, EtOH

Mittelbach et al., 1990



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Enzymes as Catalysts: Main Advantages

- Heterogenous catalysts, immobilization, reusable
- Saving of chemicals
- Easy purification of glycerol
- Catalysis of esterification as well as transesterification
- Mild reaction conditions



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Alcoholysis Without any Catalyst Supercritical Conditions

	Base catalyzed methanolysis	SCM method
Catalyst	Alkali hydroxides, alcoholates	none
Methanol amount	Slight excess	High excess
Reaction temperature [°C]	20-60	250-300
Reaction pressure [MPa]	0.1	10-25
Reaction time [min]	30-120	7-15
Free fatty acids	soaps	FAME, water
Purification of glycerol	Salt formation	No salts, possible condensation products (methyl ethers)
Energy consumption	low	high

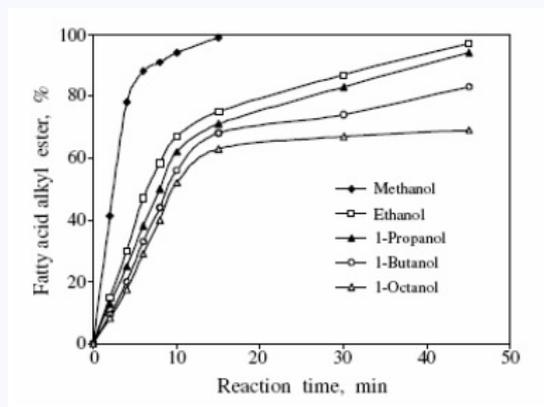


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Alcoholysis Without any Catalyst Supercritical Conditions



A.Demirbas, 2006

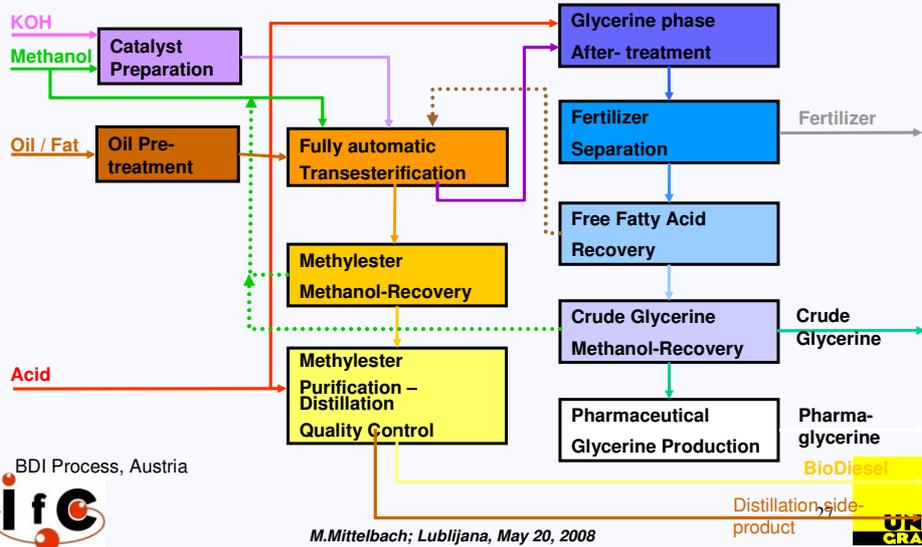


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Multi-Feedstock Production Scheme (simplified)



Thank You for Your Attention !

